

Recovery and Reuse of Chromium Ions from Tannery Wastewater by Precipitation Reaction Method

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ABSTRACT

The global concern about leather industries are increasing as leather industries grows bigger each year. These industries face very challenging task with an increase in stringent pollution control regulation enforced by various bodies due to environmental concern and human risks. The chromium salts are most widely used chemical for tanning process in leather industries, about 35% of chromium used for tanning process remain as metal and discharge to wastewater stream. The removal and recovery of this quantity of wasted chromium are necessary for environmental pollution control and economic reason. This paper shed light to chromium recovery and reuse system of Chromium salts in tanning wastewater by using NaOH as effective chemical precipitation method to regenerate chromium solution, adapted chrome recovery plant and evaluated the system technically and economically.

Key words: Chromium, precipitation, tanning, leather industries, wastewater, sodium hydroxide,

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I. INTRODUCTION

Leather industries is oldest fast growing industry as more and more different type of leather finished products needs increase that increase the growing of tanning industries in many countries. In order to improve the quality of leather, the leather cleaning and treatment process involving the following step like soaking, liming, deliming, pickling, vegetable tanning and chrome tanning industries. this processes of leather industries using high quantity of chemical like Sodium Chloride NaCl and Sodium Sulphate Na_2SO_4 and chromium and ammonium salt NH_4Cl most of this chemical discharge into waste industrial effluent which made this industries one of the heavy pollution industries containing heavy metal like chromium, copper, nickel, lead, with high concentration exceeding the discharge limit which are not easy to remove by normal treatment chromium is common pollutant in tannery industries introduce to natural water from discharge of tannery effluent to wastewater.

Chromium is one of a heavy metal found in earth's crust, Chromium exists in two oxidation states (trivalent and hexavalent state) ⁽¹⁾generally chromium found in trivalent state. The Chromium discharge to wastewater from tanning operation ⁽¹⁾.

About 30 to 40% of chromium using for chrome tanning process discharge to wastewater hence it becomes necessary to remove of the chromium from wastewater due to environmental concerns and human risks ⁽⁹⁾.

II. MATERIALS AND METHODS

Many specialized method and advanced treatment was used to remove the total chromium and hexavalent chromium from waste stream, e.g. ion exchange, membranes filtration, reverse osmosis, coagulation – flocculation, adsorption, electrocoagulation, flotation ⁽¹⁰⁾, combination of biological removal by using actinomycetes method ⁽⁷⁾ and the method of chemical precipitation Reactions ⁽⁴⁾ which becomes the most important method to remove of heavy metals, the literature showed that the percent of remove chromium from wastewater is 99% by using MgO which is more effective one among chemical precipitation method but MgO is too expensive to be economically. The precipitation reaction method of recovery and reuse of Chromium take place in the form of Chromium Hydroxide by using various agent like Magnesium Oxide, Calcium Oxide, Lime, Sodium Carbonate and Sodium Hydroxide etc. This paper shed light to

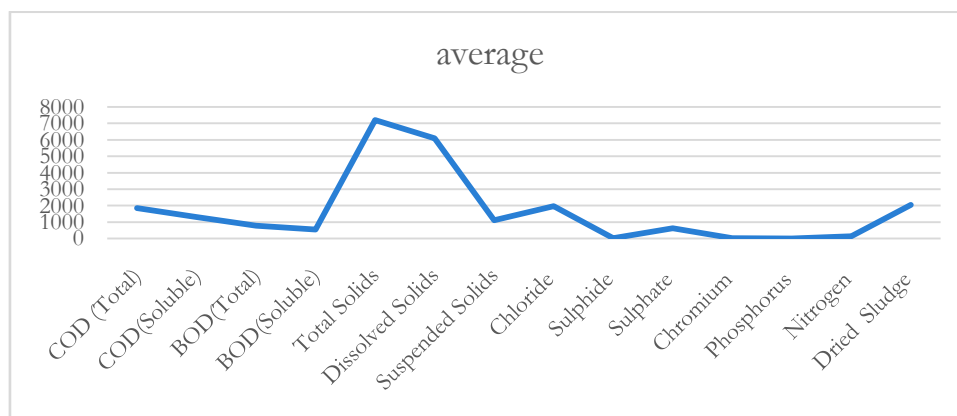
present NaOH as superior chemical precipitation method used to recover and reuse chromium from wastewater⁽⁷⁾.

Sodium Hydroxide is attempted to be a promising alternative for overcoming a Precipitation reaction method for recovery and reuse of Chromium.

the Chromium recovered by added of Sodium Hydroxide as Chromium Hydroxide, the Chromium Hydroxide is dissolved by using Sulphuric acid the recovered Chromium uses as tanning liquor⁽⁴⁾. This method is more effective and cleaner solution which can not affect the quality of leather.

Daily pollution discharge details

parameters	total pollution load
COD (Total)	1500 – 2200
COD(Soluble)	1100 – 1500
BOD(Total)	630 –930
BOD(Soluble)	440 – 670
Total Solids	5900 – 8500
Dissolved Solids	5200 – 7000
Suspended Solids	740 – 1500
Chloride	1550 – 2400
Sulphide	20 – 30
Sulphate	480 – 780
Chromium	20 – 30
Phosphorus	2 – 7
Nitrogen	110 – 190
Dried Sludge	1600 – 2500



Technology Adopted for Chrome Recovery and Reuse System

The list of equipment installed into the chrome recovery plantare stainless steel Screens fixed before the collection tank pump, effluent collection equipped with reactor and stirrer, sodium

hydroxide tank, with stirrer, chromium regeneration tank with mixer and dosing tank with dosing pump filled with Sulphuric acid and chromium liquor storage tank with Pump for regenerated chrome liquor. Figure 1-2 show process flow diagram for chrome recovery plant.

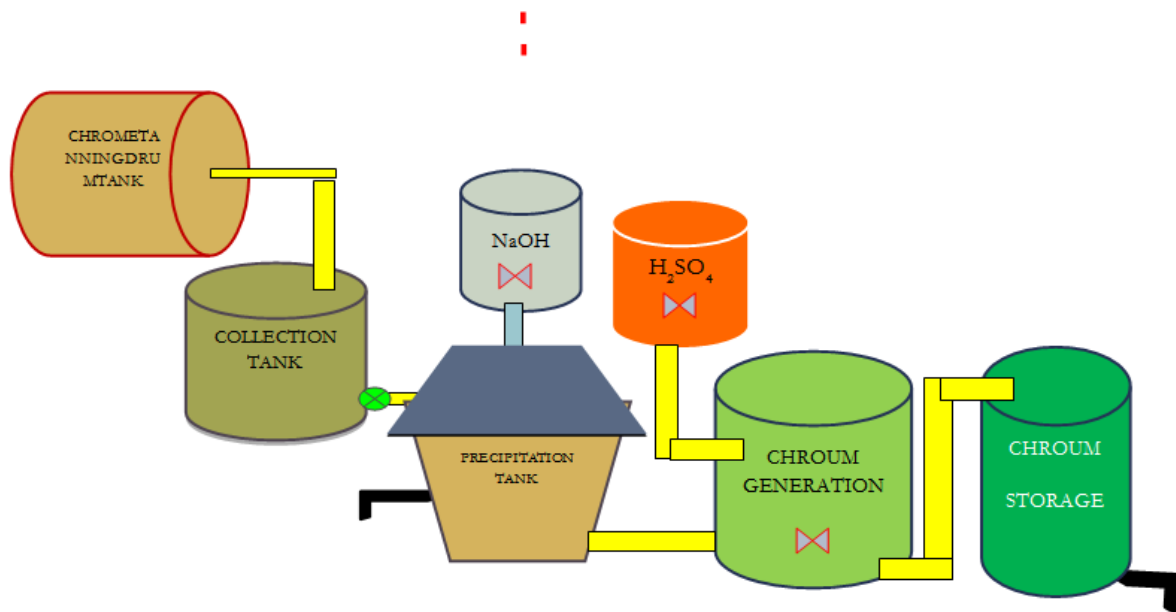


Figure (1-2) Process flow diagram for chrome recovery

Chrome Recovery Operation Procedures:

The chrome tanning drums discharge solution into chromium drain channel, tanning solution will be filtered with stainless steel screen fixed at inlet point of chrome liquor's collection tank to remove large impurities, from this point the sample was collected and used for all the tests in this study like Cr^{+3} , Cr^{+6} , biological oxygen demand (BOD) chemical oxygen demand (COD) pH, total solids, suspended solids (SS), etc. the spent tanning solution pumped by the submersible pump from collection tank into separation tank the solution then stirred with the mechanical mixer in separation tank the solution then basified to pH value of 11 by addition of caustic soda and a known quantity of calcium carbonate added to the solution with continuous stirring for a period of one hour and stopped to allow the liquor to settle for 5 hrs. The two layers of supernatant and precipitate layers are formed. The two layers will be separated. The precipitate layer which contained Chromium trivalent separated from the salt and transferred to Chromium regeneration tank and stirring by mechanical stirrer connected to Chromium regeneration tank during stirring the Sulphuric acid is added from Sulphuric acid dosing tank to acidified solution and adjust the pH range to 2-3 in regeneration tank, theoretically, Cr^{3+} removal depends in solution pH and temperature, the treated chromium is transferred to the chromium liquor storage tank.

III. FUNDAMENTAL METHOD OF PRECIPITATION:

Chemical Precipitation:

The chemistry of chromium is usually try to described clearly particularly on reaction of hexaaquachromium (III) ion $\{Cr (H_2O)_6\}^3$ complex ions with ligands of water.

To achieve stabilization, the free hexaaquachromium (III) ion $\{Cr (H_2O)_6\}^3$ Coordinated with anion containing free pairs electrons the stability depends on concentration of chromium metal and ligand, the number and orientation of and ligand of water as donor groups, the formed number and size of chelate ring and PH of solution⁽³⁾.

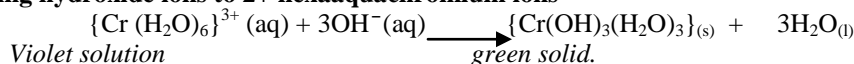
The reaction of free hexaaquachromium(III) ion $\{Cr (H_2O)_6\}^3$ with sodium hydroxide NaOH removed hydrogen ions from water ligand in the hexaaquachromium(III) ion, the hydrogen removed from the three water molecules attached to hexaaquachromium(III) ion $\{Cr (H_2O)_6\}^3$ the chromium complex become without charge (neutral complex) it will become insoluble in water and it precipitated in the solution.

Hydroxide precipitation:

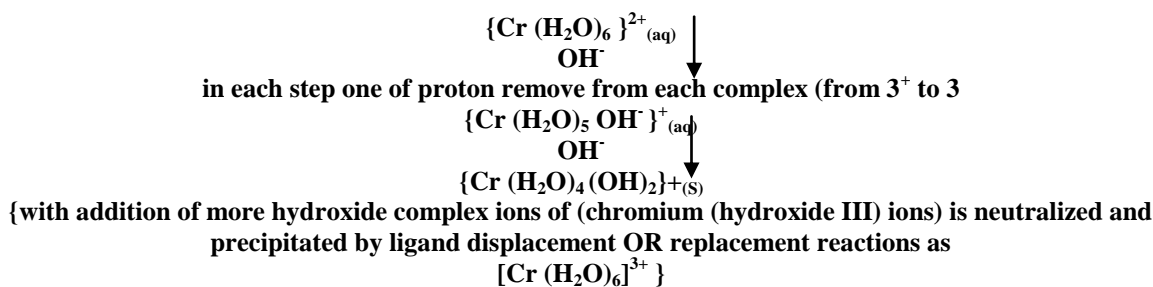
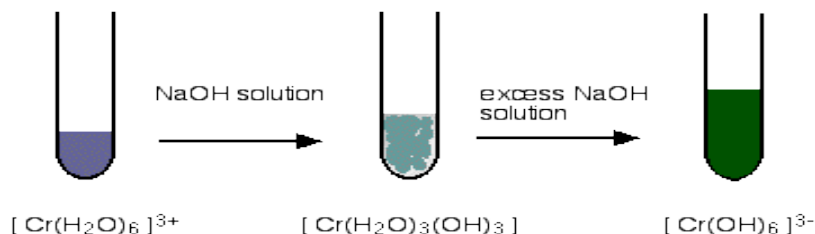
Liquor solutions contain the violet, octahedral chromium (III) ion complex react with hydroxide to form precipitate of $\{Cr(OH)_3(H_2O)_3\} (s)$

Reactions of hexaaquachromium ions with sodium hydroxide

Step-1 Adding hydroxide ions to 2+ hexaaquachromium ions



Adding hydroxide ion till new complex formed and the this formed complex is neutral compound is insoluble in water and it is precipitated in the solution.

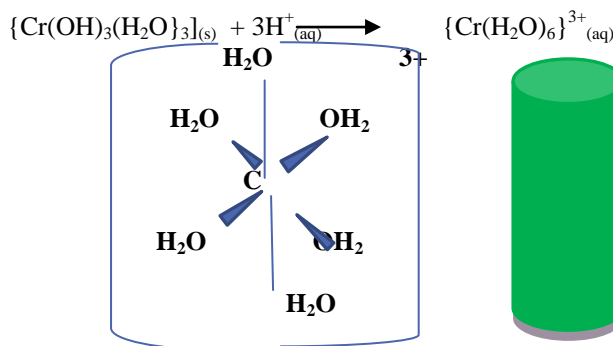


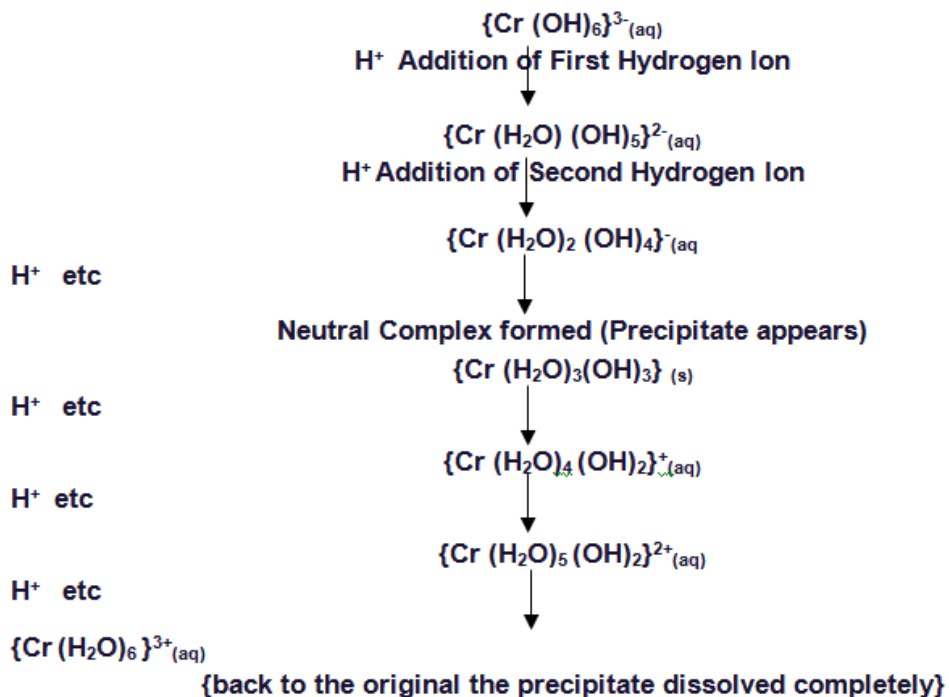
The formed precipitate of chromium hydroxide is written without including the water ligands as $Cr(OH)_2$.

Step - 2 Adding acid to hexahydroxochromate(III) ions

Chromium(III) hydroxide $[Cr(OH)_6]^{3-}$ known as an amphoteric hydroxide. Chromium(III) hydroxides because owned characteristic of amphoteric compound which may reacts with bases

(hydroxide ions) to give $[Cr(OH)_6]^{3-}$ and also when It reacts with acids like Sulphuric acid (hydrogen ions) to give $[Cr(H_2O)_6]^{3+}$. When you add Sulphuric acid decreasing pH increasing H^+ / H_3O^+ concentration and protonating the chromium (III) complex. Because the hydrogen H^+ get put back.





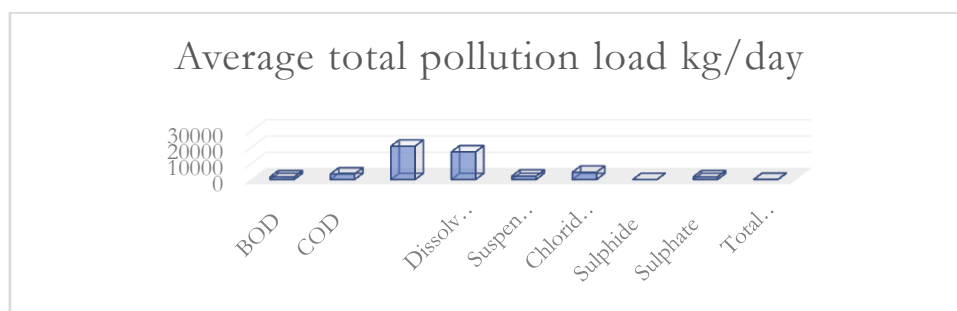
IV. RESULTS AND DISCUSSIONS

The characteristic of tanning wastewater

The tanning liquor was acidifying and treated wastewater contained concentrated Cr^{3+} , BOD, see table (1) Measurements for the inlet streams of the treatment pilot plant and chromium recovery plant.

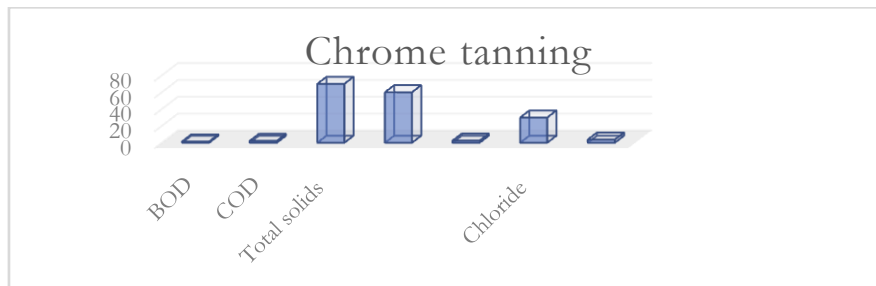
Parameters	Value	Average total pollution load kg/day
pH	9 – 7	-
BOD	1000 – 3000	1600
COD	2500 – 8000	3400
Total solid	15000 – 25000	20500
Dissolved solid	13000 – 21000	17000
Suspended solid	2000 – 4000	2100
Chloride Cl-	6000 – 9500	4500
Sulphide	30 – 50	40
Sulphate	1400 – 2000	1700
Total chromium	100 – 250	130

All value accept pH are in mg/L source of the data Al Omania for tannery and leather industries. S. Oman



Emission factors for Chrome tanning in AL Omania for tannery and leather industries.

Parameter	Chrome tanning
BOD	1.5
COD	2.2
Total solids	70
Dissolved solids	60
Suspended solids	2.5
Chloride	30
Total chromium	3.8



Cost benefitanalysis:

The cost-benefit analysis is limited by the investment, performance, maintenance costs, and supply of chemicals. The recovery of chromium is profitable. Each year, the price of the new chromium salt increases, which brings additional benefits. According to Table 4, the total capital investment in the chromium recovery system is \$ 52,000 and the annual consumption of BCS is 240 tons per year. The waste is around 80 tons. The efficiency of the Chrome recovery system is greater than 99% We can collect 90% of the fluid from the

Chrome exhaust host from Chrome Drum. Therefore, 70% of the chromium salts can be recycled and reused from a cost-benefit analysis, and you can see that the cost recovered from chromium, including all costs, is around 400US / T, while that the new chromium salt can cost more than \$ 800 / t. The recovery period for the maintenance of the vineyard is less than three years. In addition to the direct economic benefits, the cost to operators, and the maintenance of waste management facilities is low.

Total processing capacity	3000tons
Use of chromium salt (BCS)	240tons/year
Capital cost of the central chrome recovery system	52,000US\$
Annual operating cost	Cost in US Dollars
Maintenance	1,500
Labor	1,000
Chemicals	9,000
Electricity	500
Miscellaneous	2,000
Total annual operating cost	14,000
Financial cost	7,800
Depreciation	7,800
Total annual cost	29,600
benefits	-
Value of chromium recovery @ about US\$800 per ton for 70tons	\$56,000
Net profit / year	\$26,000

(UNIDO)Regional workshop on design, operation and maintenance of effluent treatment plants
 13 – 24 October 1997 – Chennai, India

V. CONCLUSIONS

Recovery of chromium(III) salts discharge through spent tanning solution from tannery effluent by using chemical precipitation reaction to precipitate chromium as chromic hydroxide($\text{Cr}(\text{HO})_3 \cdot n\text{H}_2\text{O}$ or $\text{Cr}(\text{OH})_3$ or CrH_6O_3) is performed this design show the Effect of sodium hydroxide as best precipitant coagulant which give a voluminous chromium sludge and it is therefore separate the chromium sludge by decanted the supernatant liquor and chrome slurry is dissolved in Sulphuric acid and chromium Sulphate $\{\text{Cr}_2(\text{SO}_4)_3\}$ formed again as reusable liquor. The system is more than 99% efficient in recovery chrome from chrome tanning drum the level of chromium in wastewater reduce from 100 – 150 mg/L to 10 – 20 mg/L and it re-use water and this result in increasing financial benefit addition to prevent the disbursement of chromium pollution in environment.

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